1	<u>WHA</u>	AT IS C	LAIMED IS:		
2	4		A A A A A A A A A A A A A A A A A A A		
3	1.	An integrated process for lowering the pour point of Fischer-Trop			
4		deriv	red wax which comprises:		
5					
6		(a)	collecting separately from a Fischer-Tropsch unit a		
7			Fischer-Tropsch wax and a Fischer-Tropsch condensate;		
8					
9		(b)	pyrolyzing the Fischer-Tropsch wax in a thermal cracking zone		
10			under thermal cracking conditions pre-selected to achieve a		
11			cracking conversion of the paraffins molecules present in the		
12			Fischer-Tropsch wax of at least 10 percent;		
13					
14		(c)	recovering from the thermal cracking zone a low pour point		
15			Fischer-Tropsch derived wax and a Fischer-Tropsch derived		
16			overhead product; and		
17					
18		(d)	mixing at least a portion of the Fischer-Tropsch derived		
19			overhead product recovered in step (c) and at least a portion of		
20			the Fischer-Tropsch condensate collected in step (a) with at		
21			least a portion of the low pour point Fischer-Tropsch derived		
22			wax in the proper proportion to produce a Fischer-Tropsch		
23			derived waxy product having a pour point equal to or below		
24			about 40 degrees C.		
25					
26	2.	The	The process of claim 1 wherein the thermal cracking conditions in the		
27		therr	nal cracking zone are pre-selected to achieve a cracking		
28		conv	rersion of at least 20 percent.		
29		•			
30	3.	The	The process of claim 2 wherein the thermal cracking conditions in the		
31		therr	nal cracking zone are pre-selected to achieve a cracking		
32		conv	version of at least 30 percent.		

1 4. The process of claim 3 wherein the thermal cracking conditions in the 2 thermal cracking zone are pre-selected to achieve a cracking conversion of at least 50 percent. 3 4 5 5. The process of claim 1 wherein the Fischer-Tropsch derived waxy 6 product of step (d) has a pour point below about 20 degrees C. 7 8 6. The process of claim 1 wherein the Fischer-Tropsch derived overhead 9 product of step (c) is further separated prior to step (d) into a C₅ plus 10 hydrocarbon product and a C₄ minus hydrocarbon product and the 11 C₅ plus hydrocarbon product is mixed with the Fischer-Tropsch 12 condensate and the low pour point Fischer-Tropsch derived wax in 13 step (d) to produce the Fischer-Tropsch derived waxy product. 14 15 7. The process of claim 6 wherein the C₄ minus hydrocarbon product is 16 recycled to the Fischer-Tropsch unit. 17 18 8. The process of claim 6 wherein methane is separately recovered from 19 the C₄ minus hydrocarbon product prior to the C₄ minus hydrocarbon 20 product being recycled to the Fischer-Tropsch unit and the methane is 21 recycled to a reformer for conversion into syngas for use as feed to the 22 Fischer-Tropsch unit. 23 24 9. The process of claim 1 further including the step of blending with the 25 Fischer-Tropsch waxy product a petroleum derived crude.

The process of claim 1 wherein the Fischer-Tropsch derived waxy

product also has a reduced viscosity as compared to the

26 27

28

29

10.

Fischer-Tropsch wax.

1	11.	A process for lowering the pour point of Fischer-Tropsch derived wax				
2		which comprises:				
3						
4		(a)	collecting separately from a Fischer-Tropsch unit a			
5			Fischer-Tropsch wax and a Fischer-Tropsch condensate;			
6						
7		(b)	pyrolyzing the Fischer-Tropsch wax in a thermal cracking zone			
8			under thermal cracking conditions pre-selected to achieve a			
9			cracking conversion of the paraffins molecules present in the			
10			Fischer-Tropsch wax of at least 10 percent;			
11						
12		(c)	recovering from the thermal cracking zone a thermally cracked			
13			Fischer-Tropsch derived wax intermediate having a lower pour			
14			point than the Fischer-Tropsch wax; and			
15						
16		(d)	mixing at least a portion of the Fischer-Tropsch condensate			
17			collected in step (a) with at least a portion of the thermally			
18			cracked Fischer-Tropsch derived wax intermediate in the proper			
19			proportion to produce a Fischer-Tropsch derived waxy product			
20			having a pour point equal to or below about 40 degrees C.			
21						
22	12.	The	process of claim 11 wherein the thermal cracking conditions in the			
23		therr	nal cracking zone are pre-selected to achieve a cracking			
24		conv	ersion of at least 20 percent.			
25						
26	13.	The	process of claim 12 wherein the thermal cracking conditions in the			
27		thern	nal cracking zone are pre-selected to achieve a cracking			
28		conv	ersion of at least 30 percent.			
29						
30	14.	The	process of claim 13 wherein the thermal cracking conditions in the			
31		thern	nal cracking zone are pre-selected to achieve a cracking			
32		CONV	ersion of at least 50 percent.			

1	15.	The process of claim 11 wherein the thermally cracked
2		Fischer-Tropsch derived wax intermediate has a pour point of less than
3		about 45 degrees C.
4		
5	16. `	The process of claim 11 wherein the Fischer-Tropsch derived waxy
6		product of step (d) has a pour point below about 20 degrees C.
7		
8	17.	The process of claim 11 further including the step of blending with the
9		Fischer-Tropsch waxy product a petroleum derived crude.
10		
11	18.	The process of claim 11 wherein the Fischer-Tropsch derived waxy
12		product also has a reduced viscosity as compared to the
13		Fischer-Tropsch wax.